



Requirements & KPIs

D5.1

HURRICANE

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Grant Agreement no. 101138494

Project Summary

Within HURRICANE a sector-coupling circular hub centred around the ArcelorMittal Ghent site will be created. We will target efficient resource management together with the recovery and utilization of squandered industrial waste heat and water. Together with ArcelorMittal Ghent's ongoing initiatives, this will lead to a reduction of energy, water and raw materials by at least 20%. Thanks to the ongoing projects taking place within and around the Ghent site, the site is already well connected to many other industries like waste suppliers, chemical producers (ethanol offtake & H₂ waste gas), renewable power producers, and wastewater treatment. It has become a multi-sectoral hub leading to efficient implementation of industrial symbiosis concepts. The Ghent site has a significant amount of recyclable energy, material and water that allows this symbiosis. These aspects are not only from the steel making processes, but also from other operations taking place in the mentioned "multi-sectoral" hub. This hub can be further enhanced with the integration of waste heat with its ongoing initiatives. Our solution aims at developing and demonstrating novel heat recovery (heat exchanger) and upgrading (heat pumps) solutions from selected operations and then coupling it with the internal and external off takers by means of a heat grid. With digital tools, aspects like broadening the district heating network, and adapting the heat demand profile of the buildings to better match the intermittent of the waste heat, can be optimized. Finally, an integrated software tool for circular hubs that combines the different tools and data produced at the different operations will be developed and validated. Through two virtual demonstrations and circular hubs blueprint the replication potential will be proven. The consortium is formed by 11 partners from 4 different countries, including 4 research organizations, 1 large End User, 2 SMEs, 3 civil organizations and 1 linked 3rd party.

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Executive Summary

This Key performance indicator (KPI) document is an editable document where the partners of the consortium can update the document based on the existing, newly generated data/information from the research and demonstration activities. The document is broadly divided into project KPIs and KPIs related to individual solutions. First version of this document D5.1 will be submitted as a deliverable. The report will be updated every 6 months. This document will serve as the benchmark for evaluating the findings from the project. During the demonstration campaigns the partners will evaluate the full system key performance indicators and compare it against the project objectives. This document will be adapted one last time at the end of the project as an unalterable version will be prepared as a deliverable. The HURRICANE website will also be a leading information resource for the project. ([Home - Hurricane \(hurricane-hub.eu\)](http://hurricane-hub.eu)).

2 General KPI's of the Project

| Entry | Unit | Target |
|---|---------------------------|---|
| 2.1 Operational KPI's | | |
| Capacity of the heat Grid | MW _{th} | >8 |
| Waste Heat Load available | MW _{th} | >20 |
| External Heat Demand | MWh/year | To be determined |
| Utilized waste heat | MWh/year | To be determined |
| % of heat used by internal off-takers | % | To be determined |
| % of heat used by external off-takers | % | To be determined |
| Potential Natural gas consumption avoided for external users | MWh/year | >6,500 |
| Potential light Fuel Oil (Mazout) consumption avoided | MWh/year | >2,000 |
| Potential Fuel consumption (Steam/ Blast furnace gas) avoided | MWh/year | >10,000 |
| Reduce Water consumption | m ³ /year | 30,000 |
| % of District heating capacity reached | | To be determined |
| 2.2 Environmental KPI's | | |
| Global warming | kg CO ₂ eq. | To be defined after closer study of the process |
| Acidification | kg SO ₂ eq. | To be defined after closer study of the process |
| Photo-oxidant formation | kg ethylene eq. | To be defined after closer study of the process |
| Human toxicity | 1,4-dichlorobenzene eq. | To be defined after closer study of the process |
| Freshwater aquatic ecotoxicity | 1,4-dichlorobenzene eq. | To be defined after closer study of the process |
| Eutrophication | kg PO ₄ eq. | To be defined after closer study of the process |
| Avoided CO ₂ emissions | ton CO ₂ /year | >30,000 |
| 2.3 Economical KPI's | | |
| NPV of the hub | | =0 (breakeven) |

3 Specific KPI's

3.1 Heat exchangers – Coil hot strip mill

| Entry | Unit | Target |
|---|------|---|
| Coil Hot strip mill | | |
| --% heat recovered from the coil compared to the theoretical maximum (theoretical maximum is related the difference in temperature between the initial coil temperature and the return temperature of the district heating network) | | |
| Heat Available (1 coil) | MWh | Delta T 100°C: 0.27 MWh Delta T 200°C: 0.55 MWh Delta T 300°C: 0.82 MWh Delta T 400°C: 1.09 MWh Delta T 500°C: 1.36 MWh |

| | | |
|--|------------------|---|
| Expected heat recovery with a delta T of 300°C | kWh | 245 kWh (0.88 GJ) at 30% recovery |
| Design Heat Capacity of HE | MW _{th} | To be determined |
| Max Temp | °C | 600 °C |
| Min Temp | °C | 65 °C or 338.15 K (depending on heat design capacity) |
| Pressure drops | bar | 1 (preliminary) |
| Thermal effectiveness | % | To be determined |
| heat recovered per coil | kW _{th} | To be determined |

3.2 Heat exchangers – Tunnel hot strip mill

| Entry | Unit | Target |
|--|-----------------------|--|
| Tunnel hot strip mill | | |
| ---% heat recovered from the coil compared to the theoretical maximum (theoretical maximum is related the difference in temperature between the initial coil temperature and the return temperature of the district heating network) | | |
| Heat Available when 30 coils pass in the tunnel (for 25000 coils/year) | (MW) | 0.07 MW (only radiation captured, with a radiation efficiency of 70% and an absorbance efficiency of 30%). |
| Delta T | °C | 130 °C (600°C to 470°C) |
| Expected heat recovery for one coil in the tunnel with a delta T of 130 °C (only radiation) | kWh | 4 kWh (0.014 GJ) only radiation |
| Design Heat Capacity of HE | MW _{th} | To be determined |
| Max Operating Temp | °C | 600 (Temp of Hot Coil) |
| Min. Operating Temp | °C | 65 (depending on heat design capacity) |
| Pressure drops | bar | 1 (preliminary) |
| Thermal effectiveness | % | To be determined |
| Actual heat recovered | MW _{th} /ton | To be determined |

3.3 Heat exchangers - Walking beam furnace hot strip mill

| Entry | Unit | Target |
|--|------------------|--------------------------|
| Walking beam furnace hot strip mill | | |
| Heat Available | MW _{th} | >10 |
| Delta T | °C | 5 - 20 (80°C to 75-60°C) |
| Expected heat recovery | MW _{th} | >8 |
| Max Operating Temp | °C | 81 |
| Min. Operating Temp | °C | 75 |
| Pressure drops primary side | bar | Max 0.2 |
| Thermal effectiveness | % | >95 |

3.4 Heat pump

| Entry | Unit | Target |
|----------------------------|------|-------------------------------------|
| Heat Pump | | |
| Thermal power output | kW | Above 3000 kW _{th} |
| Water Output temperature | °C | Above 120°C at the Condenser outlet |
| Coefficient of performance | - | Above 3.5 |

3.5 Software tools

| Entry | Unit | Target |
|--|------|---------------|
| EMB3R Software Platform (PDMFC) | | |
| Accuracy | % | To be defined |
| Reliability | % | To be defined |
| Predictability | % | To be defined |
| Repeatability | % | To be defined |
| Simulation timeframe | min | <15 |

| Entry | Unit | Target |
|--|------|--|
| STORM District Energy Controller | | |
| Accuracy of the waste heat forecaster compared to the monitored waste heat | | |
| Mean Absolute Error | MW | To be defined after closer study of the process and DH network |
| Mean Percentage Error | % | To be defined after closer study of the process and DH network |
| Mean Absolute Percentage Error | % | To be defined after closer study of the process and DH network |

| Entry | Unit | Target |
|--|------|--|
| Design tool for district heating networks (Pathopt) | | |
| --Capex reduction with dynamic design approach compared to a static design approach. | | |
| CAPEX Reduction of District Heating Network extension | % | To be defined after closer study of the process and DH network |
| Increase Revenue for District heating Network extension | % | To be defined after closer study of the process and DH network |

3.6 Operation heat grid

| Entry | Unit | Target |
|-------------------------|-------------------|-----------------------------|
| Performance KPIs | | |
| Capacity users Phase 1 | MWth | >8 |
| Flow max | m ³ /h | 500 |
| Max pressure | Bar | 6 |
| Temperature supply | °C | 69.5 |
| Temperature return | °C | 50-60 (depending on season) |

3.7 Socio-Economic Performance

| Entry | Unit | Target |
|--------------------------------------|------|--------|
| Performance KPIs | | |
| Stakeholders reached | No. | > 100 |
| Participants at each workshop | No. | > 20 |
| Interviews conducted | No. | 30-50 |
| Gamification tested during workshops | No. | 4 |

3.8 Dissemination

| Entry | Unit | Target |
|---|--------------------|---------------------|
| Visits (social media, website) | No. | >25.000 site visits |
| B2B | No. | >30 |
| Scientific publications | No. | >10 publications |
| Mobile application users continued engagement | % of initial users | >50 |